

Note the shift from x to x - ut, as if the origin were moving in time at speed u.

$$c(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{(x-ut)^2}{4Dt}\right)$$

If decay is also present, making the situation one of simultaneous advection-diffusion-decay, the budget equation is:

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2} - Kc$$

and the prototypical solution for an instantaneous and localized release is:

$$c(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{(x-ut)^2}{4Dt} - Kt\right)$$
decay

Higher dimensions

At 2D, with velocity vector (u, v) along axis directions x and y:

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} + v \frac{\partial c}{\partial y} = D \left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} \right)$$

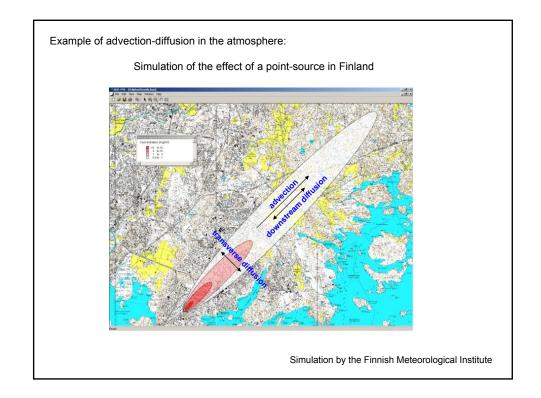
At 3D, with velocity vector (u, v, w) along axis directions x, y and z:

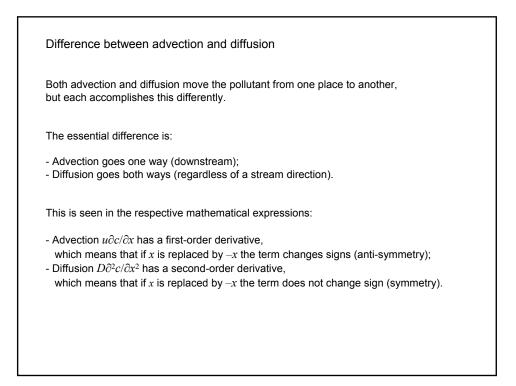
$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} + v \frac{\partial c}{\partial y} + w \frac{\partial c}{\partial z} = D \left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} + \frac{\partial^2 c}{\partial z^2} \right)$$

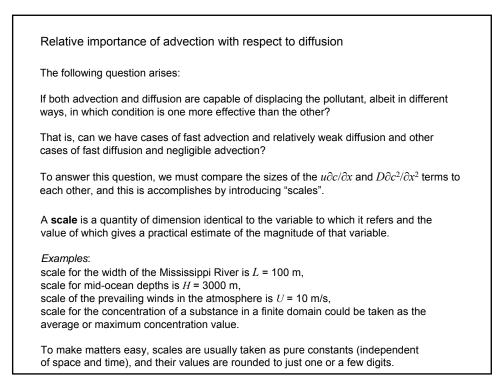
Note: An advection direction may not be active at the same time as diffusion in the same direction.

Example at 2D: If the *x*-direction is taking as the wind direction, there is no advection in the *y*-direction ($\nu = 0$), but there may still be diffusive spreading in that direction. The budget equation is then:

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} \right)$$







| VARIABLE | SCALE | CHOICE OF VALUE |
|----------|-------|--|
| С | С | Typical concentration value, such as average, initial or boundary value |
| и | U | Typical velocity value, such as maximum value |
| x | L | Approximate domain length or size of release location |

Using these scales, we can derive estimates of the sizes of the different terms.

Since the derivative $\partial c/\partial x$ is expressing, after all, a difference in concentration over a distance (in the infinitesimal limit), we can estimate it to be approximately (within 100% or so, but certainly not completely out of line with) C/L, and the advection term scales as:

$$u\frac{\partial c}{\partial x} \sim U\frac{C}{L}$$

Similarly, the second derivative $\partial^2 c/\partial x^2$ represents a difference of the gradient over a distance and is estimated at $(C/L)/L = C/L^2$, and the diffusion term scales as:

$$\frac{\partial^2 c}{\partial x^2} \sim D \frac{C}{L^2}$$

D

Equipped with these estimates, we can then compare the two processes by forming the ratio of their scales:

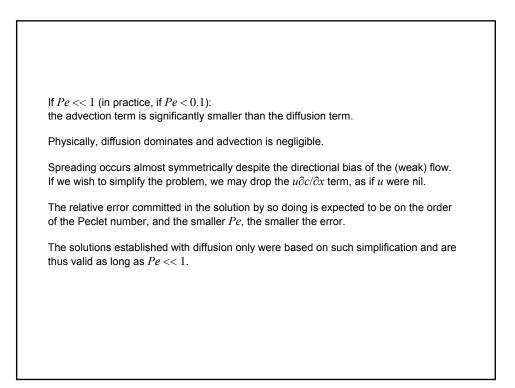
$$\frac{\text{advection}}{\text{diffusion}} = \frac{UC/L}{DC/L^2} = \frac{UL}{D}$$

This ratio is obviously dimensionless. Traditionally, it is called the Peclet number and is denoted by *Pe*:





Jean Claude Eugène Péclet (1793 – 1857)



If Pe >> 1 (in practice, if Pe > 10):

the advection term is significantly bigger than the diffusion term.

Physically, advection dominates and diffusion is negligible, and spreading is almost inexistent, with the patch of pollutant being simply moved along by the flow.

If we wish to simplify the problem, we may drop the $D\partial^2 c/\partial x^2$ term, as if *D* were nil.

The relative error committed in the solution by so doing is expected to be on the order of the inverse of the Peclet number (1/Pe), and the larger Pe, the smaller the error.

Note in this case:

that the neglect of the term with the highest-order derivative reduces the need of boundary conditions by one. No boundary condition may be imposed at the downstream end of the domain, and what happens there is whatever the flow brings.

The prototypical solution of the 1D advection only equation is:

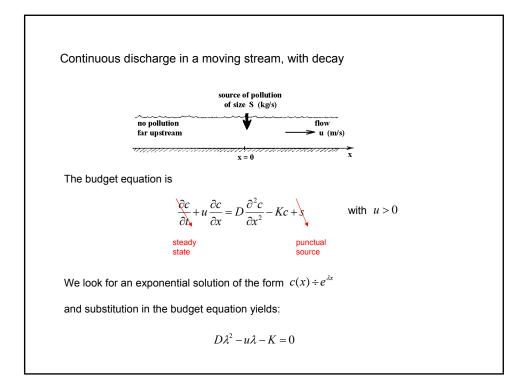
$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0 \quad \rightarrow \quad c(x,t) = c_0(x - ut)$$

in which $c_0(x)$ is the initial concentration distribution.

If $Pe \sim 1$ (in practice, if 0.1 < Pe < 10):

the advection and diffusion terms are not significantly different, and neither process dominates over the other.

No approximation to the equation can be justified, and the full equation must be utilized.



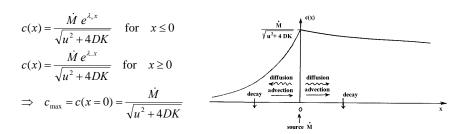
This algebraic quadratic equation possesses two solutions: $\begin{aligned} \lambda_{\star} &= \frac{u + \sqrt{u^2 + 4DK}}{2D} \\ \lambda_{-} &= \frac{u - \sqrt{u^2 + 4DK}}{2D} \end{aligned}$ The first root is always positive while the second is always negative (since u > 0). It follows that only one exponential is retained on each side of the discharge point: $c(x) = A e^{\lambda_{+}x} \quad \text{for} \quad x < 0 \\ c(x) = A e^{\lambda_{-}x} \quad \text{for} \quad x > 0 \end{aligned}$ in which the constant A of integration is the same in each expression to ensure continuity of the concentration at x = 0. The balance of fluxes in the vicinity of the source, which stipulates that what comes from the upstream side plus what comes from the source ought to be equal to what goes downstream, demands:

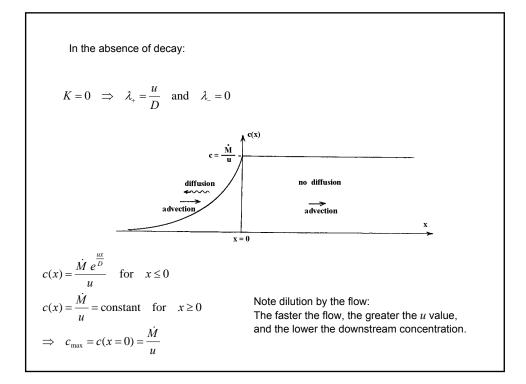
$$q(x = 0) + \dot{M} = q(x = 0) \text{ with } q = cu - D\frac{dc}{dx}$$

$$\Rightarrow (u - \lambda_{+}D) A + \dot{M} = (u - \lambda_{-}D) A$$

$$\Rightarrow A = \frac{\dot{M}}{(\lambda_{+} - \lambda_{-}) D} = \frac{\dot{M}}{\sqrt{u^{2} + 4DK}}$$

With the constant A now determined, we can write the solution:





Highly Advective Situations

Consider a 2D situation in which there is advection (direction taken as the *x*-axis) and diffusion in both downstream and transverse directions. The budget equation is:

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D\left(\frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2}\right)$$

Then assume that advection dominates over diffusion (high Peclet number). In this case, $u\partial c/\partial x$ dominates over $D\partial^2 c/\partial x^2$.

Note that we need to retain the transverse diffusion $D\partial^2 c/\partial y^2$ term since this is the only transport mechanism in that direction.

If we may further assume steady state (dc/dt = 0), then the budget equation reduces to:

$$u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial y^2}$$

which is isomorphic to the 1D diffusion-only equation

$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

by substituting $x \rightarrow ut$ and $y \rightarrow x$.

By performing the same substitution in the 1D-diffusion solution, we obtain the solution in the case of steady state advection with transverse diffusion:

$$c(x,t) = \frac{M}{\sqrt{4\pi Dt}} \exp\left(-\frac{x^2}{4Dt}\right)$$

$$x \to y \text{ and } t \to \frac{x}{u}$$
$$\longrightarrow c(x,y) = M\sqrt{\frac{u}{4\pi Dx}} \exp\left(-\frac{uy^2}{4Dx}\right)$$

The quantity M is to be interpreted as the amount of contaminant released per unit height and unit downstream direction (the "missing" dimensions z and x since diffusion operates in the y-direction).

But here the problem ought to be posed by specifying a source S per unit height and per time. The connection between the two is:

$$S = \frac{\text{amount released}}{\text{height} \times \text{time}} = \frac{\text{amount released}}{\text{height} \times \text{downstream length}} \times \frac{\text{downstream length}}{\text{time}} = M \ u$$

With S = Mu, the solution becomes:

$$c(x, y) = \frac{S}{\sqrt{4\pi Dux}} \exp\left(-\frac{uy^2}{4Dx}\right)$$

Width of spread is given by the 4σ -rule:

Width =
$$4\sigma = 5.66\sqrt{Dt} = 5.66\sqrt{\frac{Dx}{u}}$$

Example: Confluence of two streams, one of them polluted, the other clean

